

Summary of Thermo

from: first_law_rev_2005.mcd,
second_law_rev_2005.mcd,
availability.mcd
ref: van Wylen & Sonntag (eqn
#s) Woud (W nn.nn)

First Law

first law for cycle

$$\int 1 dQ = \int 1 dW \quad (5.2)$$

first law for system - change of state

$$Q_{1_2} = E_2 - E_1 + W_{1_2} \quad (5.5)$$

Q_{1_2} is the heat transferred TO system
 E_1 E_2 are initial and final values of energy of system and ...

W_{1_2} is work done BY the system

$$\delta Q = dE + \delta W = dU + dKE + dPE + \delta W \quad (5.4)$$

Closed System $\frac{d}{dt}U = \dot{Q} - \dot{W}$ $dU = \delta Q - \delta W$ $\dot{m}_e = \dot{m}_i = 0$ (W 2.3)

first law as a rate equation $\frac{d}{dt}Q = \frac{d}{dt}U + \frac{d}{dt}KE + \frac{d}{dt}PE + \frac{d}{dt}W = \frac{d}{dt}E + \frac{d}{dt}W$ (5.31 and 5.32)

first law as a rate equation - for a control volume

$H = U + p \cdot V$ enthalpy defined - is a property (5.12)
 $h = u + p \cdot v$

$$\frac{d}{dt}Q_{c_v} + \sum_n \left[\dot{m}_i \cdot \left(h_i + \frac{V_i^2}{2} + g \cdot z_i \right) \right] = \frac{d}{dt}E_{c_v} + \sum_n \left[\dot{m}_e \cdot \left(h_e + \frac{V_e^2}{2} + g \cdot z_e \right) \right] + \frac{d}{dt}W_{c_v} \quad (5.45)$$

Woud assuming energy $E = U + E_{kin} + E_{pot}$ and ... $E_{kin} = E_{pot} = 0$ $E = U$

$$\frac{d}{dt}U = \dot{Q} - \dot{W} + \dot{m}_i \cdot \left(h_i + \frac{V_i^2}{2} + g \cdot z_i \right) - \dot{m}_e \cdot \left(h_e + \frac{V_e^2}{2} + g \cdot z_e \right) \quad \text{N.B. dot} \Rightarrow \text{rate not } d(\)/dt$$

W (2.1)

steady state, steady flow process ... open stationary $\sum_n \dot{m}_i = \sum_n \dot{m}_e$ $\dot{m} = \text{flow_rate}$ (5.46)

$$\frac{d}{dt}Q_{c_v} + \sum_n \left[\dot{m}_i \cdot \left(h_i + \frac{V_i^2}{2} + g \cdot z_i \right) \right] = \sum_n \left[\dot{m}_e \cdot \left(h_e + \frac{V_e^2}{2} + g \cdot z_e \right) \right] + \frac{d}{dt}W_{c_v} \quad (5.47), (W2.8)$$

steady state steady flow ... - single flow stream

$$q + h_i + \frac{V_i^2}{2} + g \cdot z_i = h_e + \frac{V_e^2}{2} + g \cdot z_e + w$$

this on per unit mass basis $q = Q/\dot{m}$ (5.50)

uniform state, uniform flow process

$$Q_{c_v} + \sum_n \left[m_{i_n} \cdot \left(h_i + \frac{V_i^2}{2} + g \cdot z_i \right) \right] = \sum_n \left[m_{e_n} \cdot \left(h_e + \frac{V_e^2}{2} + g \cdot z_e \right) \right] \dots \tag{5.54}$$

$$+ m_2 \cdot \left(u_2 + \frac{V_2^2}{2} + g \cdot z_2 \right) - m_1 \cdot \left(u_1 + \frac{V_1^2}{2} + g \cdot z_1 \right) + W_{c_v}$$

Second Law

Carnot cycle most efficient, and only function of temperature $\eta_{\text{thermal}} = 1 - \frac{T_L}{T_H}$

Entropy inequality of Clausius ... $\int \frac{1}{T} dQ \leq 0$ **integrals are cyclic**

=> for all reversible heat engines ... $\int 1 dQ = 0$ $\int \frac{1}{T} dQ = 0$ => all irreversibles engines $\int 1 dQ \geq 0$ $\int \frac{1}{T} dQ < 0$

$dS = \left(\frac{\delta Q_{\text{rev}}}{T} \right)$ reversible ... (7.2) so as we did for energy E (e) in first law $\int \frac{1}{T} dQ$ is

$\int_1^2 \frac{1}{T} dQ_{\text{rev.}} = S_2 - S_1$ (7.3) independent of path in reversible process => is a property of the substance. entropy is an extensive property and entropy per unit mass is = s

two relationships for simple compressible substance - Gibbs equations
 equality holds when reversible and when irreversible, the change of entropy will be greater than the reversible applicable to rev & irrev processes

$$T \cdot dS = dU + p \cdot \delta V \tag{7.5} \quad T \cdot ds = du + p \cdot \delta v$$

$$T \cdot dS = dH - V \cdot dp \tag{7.6} \quad T \cdot ds = dh - v \cdot dp \tag{7.7}$$

second law for a control volume

$$\frac{d}{dt} S_{c_v} + \sum_n (m_{\text{dot}_e} \cdot s_e) - \sum_n (m_{\text{dot}_i} \cdot s_i) \geq \sum_{c_v} \frac{Q_{\text{dot}_{c_v}}}{T} \tag{7.49} \quad = \text{when reversible}$$

steady state, steady flow process $\frac{d}{dt} S_{c_v} = 0$ (7.50)

$$\sum_n (m_{\text{dot}_e} \cdot s_e) - \sum_n (m_{\text{dot}_i} \cdot s_i) \geq \sum_{c_v} \frac{Q_{\text{dot}_{c_v}}}{T} \tag{7.51} \quad = \text{when reversible}$$

uniform state, uniform flow process

$$m_2 \cdot s_2 - m_1 \cdot s_1 + \sum_n (m_e \cdot s_e) - \sum_n (m_i \cdot s_i) \geq \int_0^t \frac{Q_{\text{dot}_{c_v}}}{T} dt \tag{7.56} \quad = \text{when reversible}$$

Availability

reversible work (maximum) of a control volume that exchanges heat with the surroundings at T_o

$$W_{rev} = \sum_n \left[m_{i_n} \cdot \left(h_i - T_o \cdot s_i + \frac{V_i^2}{2} + g \cdot z_i \right) \right] - \left[\sum_n \left[m_{e_n} \cdot \left(h_e - T_o \cdot s_e + \frac{V_e^2}{2} + g \cdot z_e \right) \right] \right] \quad (8.7)$$

latter [...] is total for c.v.

$$+ \left[m_2 \cdot \left(u_2 - T_o \cdot s_2 + \frac{V_2^2}{2} + g \cdot z_2 \right) \right] - m_1 \cdot \left(u_1 - T_o \cdot s_1 + \frac{V_1^2}{2} + g \cdot z_1 \right)$$

system (fixed mass)

$$\frac{W_{rev_1_2}}{m} = w_{rev_1_2} = \left(u_1 - T_o \cdot s_1 + \frac{V_1^2}{2} + g \cdot z_1 \right) - \left(u_2 - T_o \cdot s_2 + \frac{V_2^2}{2} + g \cdot z_2 \right) \quad (8.8)$$

steady-state, steady flow process - rate form

$$W_{\dot{rev}} = \sum_n \left[m_{i_n} \cdot \left(h_i - T_o \cdot s_i + \frac{V_i^2}{2} + g \cdot z_i \right) \right] - \left[\sum_n \left[m_{e_n} \cdot \left(h_e - T_o \cdot s_e + \frac{V_e^2}{2} + g \cdot z_e \right) \right] \right] \quad (8.9)$$

single flow of fluid

$$\frac{W_{\dot{rev}}}{m_{\dot{}}} = w_{rev} = h_i - T_o \cdot s_i + \frac{V_i^2}{2} + g \cdot z_i - \left(h_e - T_o \cdot s_e + \frac{V_e^2}{2} + g \cdot z_e \right) \quad (8.10)$$

availability

steady state, steady flow process ... (e.g. single flow ... availability (per unit mass flow))

$$\psi = h - T_o \cdot s + \frac{V_i^2}{2} + g \cdot z - \left(h_o - T_o \cdot s_o + \frac{V_o^2}{2} + g \cdot z_o \right) \quad (8.16)$$

reversible work between any two states = decrease in availability between them

$$w_{rev} = \psi_i - \psi_e = h_1 - T_o \cdot s_1 - h_2 + T_o \cdot s_2 = h_1 - T_o \cdot s_1 - h_2 + T_o \cdot s_2 = (h_1 - h_2) - T_o \cdot (s_1 - s_2) \quad (8.17) \text{ extended}$$

can be written for more than one flow ...

$$W_{\dot{rev}} = \sum_n (m_{i_n} \cdot \psi_{i_n}) - \sum_n (m_{e_n} \cdot \psi_{e_n}) \quad (8.18)$$

availability w/o KE and PE per unit mass of system

$$\phi = (u + p_0 \cdot v - T_0 \cdot s) - (u_0 + p_0 \cdot v_0 - T_0 \cdot s_0) = u - u_0 + p_0 \cdot (v - v_0) - T_0 \cdot (s - s_0) \quad (8.21)$$

and reversible work maximum between states 1 and 2 is ...

$$w_{\text{rev}_1_2} = \phi_1 - \phi_2 - p_0 \cdot (v_1 - v_2) + \frac{V_1^2 - V_2^2}{2} + g \cdot (z_1 - z_2) \quad (8.22)$$